

IN THE CLAIMS

Please amend the claims as follows:

Claim 1 (Currently Amended): A process for preparing a silicon compound bearing at least one fluoroalkyl group by hydrosilylation of a fluoroolefin in the presence of a Pt-containing hydrosilylation catalyst, the process comprising:

- initially charging and heating a hydrogenchlorosilane;
- metering in the fluoroolefin and reacting the reaction mixture; and
- subsequently isolating the hydrosilylation product, and

wherein the Pt-containing hydrosilylation catalyst consists of a hexachloroplatinic acid or a Pt(0) complex;

wherein the fluoroolefin has an iodine content of less than 170 ppm by weight, a diene content of less than 100 ppm by weight, and a water content of less than 100 ppm by weight.

Claim 2 (Previously Presented): The process as claimed in claim 1, wherein,

- (i) the hydrogenchlorosilane is initially charged, heated, the hydrosilylation catalyst dissolved in an inert solvent is added and the fluoroolefin is then metered in; or
- (ii) the hydrogenchlorosilane is initially charged, heated and a mixture of fluoroolefin, hydrosilylation catalyst and optionally solvent is metered in; or
- (iii) a mixture of the hydrogenchlorosilane and the hydrosilylation catalyst dissolved in a solvent are initially charged, heated, and the fluoroolefin is metered in.

Claim 3 (Previously Presented): The process as claimed in claim 1, wherein the initially charged hydrogen-chlorosilane or the initially charged hydrogenchlorosilane-containing mixture is heated to a temperature in the range from 85 to 120°C.

Claim 4 (Previously Presented): The process as claimed in claim 1, wherein hydrogenchlorosilane and fluoroolefin are used in a molar ratio of from 3:1 to 0.5:1.

Claim 5 (Previously Presented): The process as claimed in claim 1, wherein toluene or xylene is used as an inert solvent.

Claim 6 (Previously Presented): The process as claimed in claim 1, wherein the catalyst is used in a molar ratio of Pt to hydrogenchlorosilane of from 1:100 000 to 1:100.

Claim 7 (Previously Presented): The process as claimed in claim 1, wherein at least one hydrogenchlorosilane of the formula (I)



wherein the groups R are identical or different and R is a linear, branched or cyclic alkyl group having from 1 to 20 carbon atoms or an aryl group,

the X is Cl,

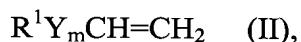
a = 0, 1, 2 or 3,

b = 0, 1, 2 or 3, and

1 $\leq (a+b) \leq 3$.

Claims 8-11 (Cancelled).

Claim 12 (Previously Presented): The process as claimed in claim 1, wherein at least one fluoro-olefin of the formula II



wherein R¹ is a monofluorinated, oligofluorinated, or perfluorinated alkyl group having from 1 to 12 carbon atoms or a perfluorinated aryl group, Y is a -CH₂-, -O-, -O-CH₂-, or -S-group, and m is 0 or 1.

Claim 13 (Previously Presented): The process as claimed in claim 1, wherein the fluoroolefin is selected from the group consisting of

3,3,3-trifluoro-1-propene,

3,3,4,4,5,5,6,6,7,7,8,8,8-tridecafluorooctene,

3,3,4,4,5,5,6,6,7,7,8,8,9,9,10,10,10-tridecafluorooccene,

1,1,2,2-tetrafluoroethyl allyl ether,

3,3,4,4,5,5,6,6,7,7,8,8,9,9,10,10,10-heptadecafluorodecene,

3,3,4,4,5,5,6,6,7,7,8,8,9,9,10,10,11,11,12,12,12-hencosafluorooctene, and

3,3,4,4,5,5,6,6,7,7,8,8,9,9,10,10,11,11,12,12,13,13, 14,14,14-pentacosafluorooctene.

Claim 14 (Previously Presented): The process as claimed in claim 1, wherein the fluoroolefin is added to the initially charged hydrogenchlorosilane as set forth in (i) or (ii) or (iii) at a pressure of from 1 to 15 bar abs.

Claim 15 (Previously Presented): The process as claimed in claim 1, wherein the fluoroolefin is metered in at a rate of from 50 to 300 l/h, based on 1 t of chlorosilane.

Claim 16 (Previously Presented): The process as claimed in claim 1, wherein the reaction is carried out at a temperature in the range from 85 to 120°C and a pressure of from 1.5 to 50 bar abs. for a period of from 4 to 20 hours.

Claim 17 (Previously Presented): The process as claimed in claim 1, wherein the hydrosilylation product is isolated from the product mixture by distillation and is subsequently esterified with an alcohol, wherein the alcohol is used in an excess of from 0.1 to 10% and the alcohol used is denatured with ≤ 1 % by weight of methyl ethyl ketone or petroleum ether.

Claim 18 (Previously Presented): The process as claimed in claim 1 performed batchwise in a stirred tank reactor.